## AIR-STEAM SYSTEM PRODUCES THE DELICIOUS!!

EFFECTIVE DESIGHN NEEDS LESS SPACE \& SAVES ENERGY!!


EXAMPLE
KYUNGHAN Co., Ltd.

## STERI-ACE REQURED UTILITIES

|  | PRS-10-I | PRS-20-I | PRS-30-I | PRS-40-I |
| :---: | :---: | :---: | :---: | :---: |
| COMPRESSOR | $3.7 \mathrm{KW}(5 \mathrm{HP})$ | 5.5KW(7.5HP) | 7.5KW( 10HP) | 11 KW (15HP) |
| AIR RESERVOIR TANK | TANK LEVEL UP | 1000 l | 1300 l | 1500 l |
| AIR INLET | 10A | 10A | 10A | 10A |
| COOLING WATER SUPPLY PUMP | 1HP 1PHASE | 2 HP 1PHASE | 3HP 3PHASE | 3HP 3PHASE |
| COOLING WATER INLET | 20A | 40A | 50A | 50A |
| COOLING WATER TANK | 1 TON | 2 TON | 3 TON | 4 TON |
| BOILER | $300 \mathrm{~kg} / \mathrm{hr}$ | $500 \mathrm{~kg} / \mathrm{hr}$ | $800 \mathrm{~kg} / \mathrm{hr}$ | $1000 \mathrm{~kg} / \mathrm{hr}$ |
| STEAM INLET | 25 A | 40A | 50A | 50A |
| SIZE OF VESSEL ( $W * H *$ ) | $750 * 1030 * 1260$ | 750*20471260 | $750 * 3037 * 1260$ | $750 * 4047 * 1260$ |
| CHAMBER SIZE ( $W$ *H*L) | $620 * 950 * 960$ | $620 * 1900 * 960$ | $620 * 2850 * 960$ | $620 * 3800 * 960$ |
| DIMENSION ( $W$ * $\mathrm{H} * \mathrm{~L}$ ) | $1700 * 1400 * 2150$ | $1700 * 1400 * 2150$ | 1850*3400*2200 | $1850 * 4400 * 2400$ |

## STERI-ACE SPECIFICATION

|  | PRS-10-I | PRS-20-I | PRS-30-I | PRS-40-I |
| :---: | :---: | :---: | :---: | :---: |
| MAX. WORKING PRESS•TEMP (kg/ $\mathrm{cm}^{3} \mathrm{G},{ }^{\circ} \mathrm{C}$ ) | $2.0 / 125^{\circ} \mathrm{C}$ |  |  |  |
| CHAMBER VOLUME ( $\ell$ ) | 1035 | 1975 | 2920 | 3850 |
| WEIGHT OF EQUIPMENT(kg) | 1850 | 2500 | 3200 | 4000 |
| STEAM CONSUMPTION(kg/1batch) | 65 | 125 | 200 | 300 |
| REQUIRED STEAM ( $\mathrm{kg} / \mathrm{Hr}$ ) | $200 \mathrm{~kg} / \mathrm{hr} \mathrm{MIN}$. | $400 \mathrm{~kg} / \mathrm{hr} \mathrm{MIN}$. | $600 \mathrm{~kg} / \mathrm{hr} \mathrm{MIN}$. | $800 \mathrm{~kg} / \mathrm{hr} \mathrm{MIN}$. |
| COOLING WATER ( $\ell / 1$ batch. 15 min.$)$ | 300 | 600 | 900 | 1200 |
| REQUIRED COMPRESSOR(kW) | 3.7 | 5.5 | 7.5 | 11 |
| NO. OF CART | 1 | 2 | 3 | 4 |
| DIMENSION OF CHAMBER $W *$ **H(mm) | $620 * 950 * 960$ | $620 * 1900 * 960$ | $620 * 2850 * 960$ | $620 * 3800 * 960$ |
| DIMENSION OF MACHINE W*L*H(mm) | 1680*1365*2150 | 1680*2365*2150 | 1680*3365*2300 | 1680*4365*2400 |
| Tray ( 30 mm 기준) | 32TRAYS* 1SET | 32TRAYS*2SET | 32TRAYS*3SET | 32TRAYS*4SET |
| NO. OF POUCH ( 130*170*20(mm) | 768POUCH/ 1Batch | 1536POUCH/ 1Batch | 2304POUCH/ 1Batch | 3072POUCH/ 1Batch |
| CAPACITY ( $200 \mathrm{~g} /$ pouch) | $153 \mathrm{~kg} /$ 1Batch | $307 \mathrm{~kg} /$ 1Batch | $460 \mathrm{~kg} /$ 1Batch | $614 \mathrm{~kg} / 1$ Batch |



## 「 STERI-ACE 」 WORKING PRINCIPLE

An air steam type retort sterilizer, STERI-ACE, was developed on the foundation of an autoclave that are used in pharmaceutical industries. The drawback from existing steam type and retort sterilizer which is ununiformity of temperature distribution inside of chamber due to Air Pocket.

## 「 STERI-ACE 」 WORKING PRINCIPLE

Sterilization process of STERI-ACE is divided into 4 major steps as Exhaustion, Ascension, Sterilization, Cooling and Drain.

Ascension and Sterilization process also be divided into 1st Ascension, 1st Sterilization, 2nd Ascension and 2nd Sterilization since STERI-ACE adopted Two Step Sterilization to maximize its efficiency.

## EXHAUSTION PROCESS

Purpose of Exhaustion Process is to eliminate cooled and dry air inside of chamber with saturated steam to make adequate environment for sterilization. During the Exhaustion Process, a cold air or not yet heated air inside of chamber will be exchanged with preheated air and saturated steam continuously until temperature of chamber reaches set temperature.

## STERILIZATION PROCESS

After Exhaustion Process is completed, STERI-ACE will proceed with Ascension Process. For STERI-ACE, it is very short since medium for heating is steam instead of heated water.

When the temperature of chamber reaches target temperature, timer will automatically start. During the Sterilization process, steam will be supplied continuously in the manner of forced circulation by suction.

## COOLING PROCESS

For the Cooling Process, a primary purpose of this cooling process is to prevent pouch from rupturing. During the Sterilization process, the contents inside of pouch has been already boiled and the air has been expended due temperature. If the chamber door is opened without cooling down the products, the pouch will rupture due to differences between pressure inside of pouch and outside.

However, the temperature of product cool down before they are out of chamber, pressure balance will prevent from the rupture. Moreover, cooling process also can be used in actual cooling of product.


## CYLNDRICAL VS. RECTANGULAR

Most of Retort Sterilizers have Circular shape Chamber. However, STERI-ACE of Kyunghan Co., Ltd. has Rectangular shape of Chamber which is space and energy efficient.

For Circular shape chamber, chamber itself does not require reinforcement as much as rectangular shape chamber since circular shape itself is structurally pressure resistant. For the manufacturer, it is cost saving since it requires less reinforcement as mentioned above. However, it has more dead space than a rectangular structure.

## CYLINDRICAL STRUCTURE

Dimension of Cylindrical Chamber (mm): Ø1370 x 4000

Tray Loading Dimension (mm): (900 x $980 \times 900) \times 4$ sets
Volume of Cylindrical Chamber: Vol $\mathbf{C}\left(\mathrm{m}^{3}\right)=\pi / 4 * \mathrm{D}^{2} * \mathrm{~L}$

$$
=\pi / 4 * 2.15 * 3.10
$$

$$
=5.90
$$

Volume of Trays: Vol T $\left(\mathrm{m}^{3}\right)=(0.90 * 0.98 * 0.90) * 4$

$$
=3.18
$$

Dead Space cylindrical $\left(m^{3}\right)=$ Chamber Volume $\left(m^{3}\right)-$ Tray Loading Volume $\left(m^{3}\right)$

$$
\begin{aligned}
& =\text { Vol C }- \text { Vol T } \\
& =5.90-3.18 \\
& =2.72
\end{aligned}
$$

## RECTANGULAR STRUCTURE

Chamber Dimension (mm): $750 \times 1260 \times 4100$
Tray Loading Dimension (mm): (640 x $960 \times 960) \times 4$ sets
Volume of Rectangular Chamber: Vol R $\left(m^{3}\right)=0.75 * 1.26 * 4.10$

$$
=3.87
$$

Volume of Trays: Vol T $\left(\mathrm{m}^{3}\right)=(0.64 * 0.96 * 0.96) * 4$

$$
=2.36
$$

Dead space rectangular $\left(m^{3}\right)=$ Chamber Volume $\left(m^{3}\right)-\operatorname{Tray} \operatorname{Volume}\left(m^{3}\right)$

$$
=\operatorname{Vol} \mathbf{R}-\operatorname{Vol} T
$$

$$
=3.87-2.36
$$

$$
=1.51
$$

## RECTANGULAR STRUCTURE

Dead Space cylindrical $\left(m^{3}\right)=$ Chamber Volume $\left(m^{3}\right)-$ Tray Loading Volume $\left(m^{3}\right)$

$$
\begin{aligned}
& =\text { Vol C }- \text { Vol T } \\
& =5.90-3.18 \\
& =2.72
\end{aligned}
$$

Dead space rectangular $\left(m^{3}\right)=$ Chamber Volume $\left(m^{3}\right)-\operatorname{Tray} \operatorname{Volume}\left(m^{3}\right)$

$$
\begin{aligned}
& =\mathbf{V o l} \mathbf{R}-\mathbf{V o l ~ T} \\
& =3.87-2.36 \\
& =\mathbf{1 . 5 1}
\end{aligned}
$$

Dead Space rectangular $1.15\left(\mathrm{~m}^{3}\right)<$ Dead Space cylindrical $2.72\left(\mathrm{~m}^{3}\right)$
Therefore, Rectangular structure is more efficient than cylindrical structure.



## 

Data Values

|  | Deg C | ForDit |
| :---: | :---: | :---: |
| $01 / 2$ | 121.6 | Pref |
| 02 R | 121.6 | SRef |
| 030 | 121.7 | 0.1 |
| 04 D | 1218 | 0.2 |
| 050 | 121.5 | -0.1 |
| 060 | 121.6 | 0.0 |
| 070 | 121.2 | 0.0 |
| 080 | 122.1 | 0.5 |
| 090 | 121.7 | 0.1 |
| 100 | 1220 | 04 |
| 110 | 121.6 | 0.0 |
| 12 D | 121.8 | 0.2 |
| 130 | 121.6 | 00 |
| 14 D | 121.1 | -0.5 |
| 15 D | 121.2 | -0.4 |
| 16 D | 120.8 | $-0.7$ |
| feating |  | Scan z |


|  | Degc | Folder |
| :---: | :---: | :---: |
| 17 D | 121.7 | 0.1 |
| 188 | 121.5 | -0.1 |
| 190 | 121.3 | -0.3 |
| 200 | 120.9 | -0.7 |
| 210 | 121.4 | -0.2 |
| 22 D | 121.2 | -0.4 |
| 23 D | 1209 | -0.7 |
| 240 | 121.2 | -0.4 |
| 250 | 121.0 | -0.6 |
| 260 | 121.0 | -0.6 |
| 27 D | 121.1 | -0.5 |
| 28 D | 121.0 | -0.6 |
| 29 D | 1209 | -0.7 |
| 300 | 1209 | -0.7 |
| 310 | 121.2 | -0.4 |
| 320 | 121.1 | -0.5 |
| W19 | Stat | 12890 |



Data Display Mode
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Probe Teat


KYUNGHAN Co., Ltd.


