

#### AIR-STEAM SYSTEM PRODUCES THE DELICIOUS!! EFFECTIVE DESIGHN NEEDS LESS SPACE & SAVES ENERGY!!



#### **STERI-ACE REQURED UTILITIES**

	PRS-10-I	PRS-20-I	PRS-30-I	PRS-40-I
COMPRESSOR	3.7KW(5HP)	5.5KW(7.5HP)	7.5KW(10HP)	11KW(15HP)
AIR RESERVOIR TANK	TANK LEVEL UP	1000 <i>l</i>	1300 <i>l</i>	1500 <i>l</i>
AIR INLET	10A	10A	10A	10A
COOLING WATER SUPPLY PUMP	1HP 1PHASE	2HP 1PHASE	3HP 3PHASE	3HP 3PHASE
COOLING WATER INLET	20A	40A	50A	50A
COOLING WATER TANK	1 TON	2 TON	3 TON	4 TON
BOILER	300kg/hr	500kg/hr	800kg/hr	1000kg/hr
STEAM INLET	25A	40A	50A	50A
SIZE OF VESSEL (W*H*L)	750*1030*1260	750*20471260	750*3037*1260	750*4047*1260
CHAMBER SIZE (W*H*L)	620*950*960	620*1900*960	620*2850*960	620*3800*960
DIMENSION (W*H*L)	1700*1400*2150	1700*1400*2150	1850*3400*2200	1850*4400*2400

#### **STERI-ACE SPECIFICATION**

	PRS-10-I	PRS-20-I	PRS-30-I	PRS-40-I
MAX. WORKING PRESS·TEMP (kg/ ☞Ĝ, ℃)		2.0 /	125℃	
CHAMBER VOLUME( 1)	1035	1975	2920	3850
WEIGHT OF EQUIPMENT(kg)	1850	2500	3200	4000
STEAM CONSUMPTION(kg/1batch)	65	125	200	300
REQUIRED STEAM (kg/Hr)	200kg/hr MIN.	400kg/hr MIN.	600kg/hr MIN.	800kg/hr MIN.
COOLING WATER (ℓ/1batch.15min.)	300	600	900	1200
REQUIRED COMPRESSOR(KW)	3.7	5.5	7.5	11
NO. OF CART	1	2	3	4
DIMENSION OF CHAMBER W*L*H(mm)	620*950*960	620*1900*960	620*2850*960	620*3800*960
DIMENSION OF MACHINE W*L*H(mm)	1680*1365*2150	1680*2365*2150	1680*3365*2300	1680*4365*2400
Tray (30mm기준)	32TRAYS*1SET	32TRAYS*2SET	32TRAYS*3SET	32TRAYS*4SET
NO.OF POUCH(130*170*20(mm)	768POUCH/1Batch	1536POUCH/1Batch	2304P0UCH/1Batch	3072P0UCH/1Batch
CAPACITY (200g/pouch)	153kg/1Batch	307kg/1Batch	460kg/1Batch	614kg/1Batch



# **STERI-ACE J WORKING PRINCIPLE**

An air steam type retort sterilizer, STERI-ACE, was developed on the foundation of an autoclave that are used in pharmaceutical industries. The drawback from existing steam type and retort sterilizer which is ununiformity of temperature distribution inside of chamber due to Air Pocket.

# **STERI-ACE J WORKING PRINCIPLE**

Sterilization process of STERI-ACE is divided into 4 major steps as Exhaustion, Ascension, Sterilization, Cooling and Drain.

Ascension and Sterilization process also be divided into 1st Ascension, 1st Sterilization, 2nd Ascension and 2nd Sterilization since STERI-ACE adopted Two Step Sterilization to maximize its efficiency.

#### **EXHAUSTION PROCESS**

Purpose of Exhaustion Process is to eliminate cooled and dry air inside of chamber with saturated steam to make adequate environment for sterilization. During the Exhaustion Process, a cold air or not yet heated air inside of chamber will be exchanged with preheated air and saturated steam continuously until temperature of chamber reaches set temperature.

#### **STERILIZATION PROCESS**

After Exhaustion Process is completed, STERI-ACE will proceed with Ascension Process. For STERI-ACE, it is very short since medium for heating is steam instead of heated water.

When the temperature of chamber reaches target temperature, timer will automatically start. During the Sterilization process, steam will be supplied continuously in the manner of forced circulation by suction.

# **COOLING PROCESS**

For the Cooling Process, a primary purpose of this cooling process is to prevent pouch from rupturing. During the Sterilization process, the contents inside of pouch has been already boiled and the air has been expended due temperature. If the chamber door is opened without cooling down the products, the pouch will rupture due to differences between pressure inside of pouch and outside.

However, the temperature of product cool down before they are out of chamber, pressure balance will prevent from the rupture. Moreover, cooling process also can be used in actual cooling of product.



#### **CYLNDRICAL VS. RECTANGULAR**

Most of Retort Sterilizers have Circular shape Chamber. However, STERI-ACE of Kyunghan Co., Ltd. has Rectangular shape of Chamber which is space and energy efficient.

For Circular shape chamber, chamber itself does not require reinforcement as much as rectangular shape chamber since circular shape itself is structurally pressure resistant. For the manufacturer, it is cost saving since it requires less reinforcement as mentioned above. However, it has more dead space than a rectangular structure.

#### **CYLINDRICAL STRUCTURE**

Dimension of Cylindrical Chamber (mm): Ø1370 x 4000

Tray Loading Dimension (mm): (900 x 980 x 900) x 4 sets

Volume of Cylindrical Chamber: Vol C( $M^3$ ) =  $\pi/4 * D^2 * L$ =  $\pi/4 * 2.15 * 3.10$ = 5.90

Volume of Trays: Vol T ( $\mathbb{M}^3$ ) = (0.90 \* 0.98 \* 0.90) \* 4 = 3.18

**Dead Space cylindrical**  $(\mathbb{M}^{\circ})$  = Chamber Volume $(\mathbb{M}^{\circ})$  – Tray Loading Volume $(\mathbb{M}^{\circ})$ = Vol C – Vol T = 5.90 – 3.18 = 2.72

#### **RECTANGULAR STRUCTURE**

Chamber Dimension (mm): 750 x 1260 x 4100

Tray Loading Dimension (mm): (640 x 960 x 960) x 4 sets

Volume of Rectangular Chamber: Vol R ( $M^3$ ) = 0.75 \* 1.26 \* 4.10 = 3.87

Volume of Trays: Vol T ( $\mathbb{M}^3$ ) = (0.64 \* 0.96 \* 0.96) \* 4 = 2.36

Dead space rectangular ( $\mathbb{M}^3$ ) = Chamber Volume( $\mathbb{M}^3$ ) – Tray Volume( $\mathbb{M}^3$ ) = Vol R – Vol T = 3.87 – 2.36 = 1.51

#### **RECTANGULAR STRUCTURE**

**Dead Space cylindrical**  $(\mathbb{M}^{\circ})$  = Chamber Volume $(\mathbb{M}^{\circ})$  - Tray Loading Volume $(\mathbb{M}^{\circ})$ = Vol C - Vol T = 5.90 - 3.18 = 2.72

Dead space rectangular ( $\mathbb{M}^3$ ) = Chamber Volume( $\mathbb{M}^3$ ) – Tray Volume( $\mathbb{M}^3$ ) = Vol R – Vol T = 3.87 – 2.36 = 1.51

Dead Space rectangular 1.15 ( $m^{\circ}$ ) < Dead Space cylindrical 2.72 ( $m^{\circ}$ )

Therefore, Rectangular structure is more efficient than cylindrical structure.







Data Va	alues					Data Aquisition	
	Deg C	ForDitt		Deg C	Fo/Diff	(an Data	Transfer 1 18
01 R	121.6	PRet	17 D	121.7	0.1	Log Data	Target Eo
02 R	121.6	S Ref	18 D	121.5	-0.1	End Come Ha	PRaf 3
03 D	121.7	0.1	19 D	121.3	-0.3	e connerte en	
04 D	121.8	0.2	20 D	120.9	-0.7	End Heating	Scan Rate
05 D	121.5	+0.1	21 0	121.4	-0.2	- Constrainty	Contraction of the local division of the loc
06 D	121.6	0.0	22 D	121.2	-0.4	Out	Data Display Mode
07 D	121.2	-0.4	23 D	120.9	-0.7		Calbrated CRaw
08 D	122.1	0.5	24 D	121.2	-0.4	Restart	Trace of the second sec
09 D	121.7	0.1	25 D	121.0	-0.6		Drohe Test
10 D	122.0	0.4	26 D	121.0	-0.6		THEFTER
11 D	121.6	0.0	27 D	121.1	-0.5	Pre-Test Calibratio	anna Clahilhu
12 D	121.8	0.2	28 D	121.0	-0,6	Manual 121	6 0.6 Calibrate
13 D	121.6	0.0	29 D	120.9	-0.7		
14 D	121.1	-0.5	30 D	120.9	-0.7	In-Process Calibra	son
15 D	121.2	-0.4	31 D	121.2	-0.4	C Manual Case	ence Stability Calibrate
16 D	120.9	-0.7	32 D	121.1	-0.5	121	6 0.0
Heating		Scan #	119	Start	12:59:02	Next 13:28:47	13.28.37 Elapsed 29.58
Contraction of the second			-	-			
				5			

